

TABLE 1. GALVANIC CURRENT AND POTENTIAL MEASUREMENTS AT 4 °C

Galvanic Couple (Anode/Cathode)	Area Ratio	Couple Potential (mV)	Galvanic Current Density ($\mu\text{A}/\text{cm}^2$)
Al/Type 316L SS	1:1	-757.2	105.7
Al/Type 316L SS	10:1	-784.0	165.9
Al/NAB	1:1	-557.4	142.1
Al/NAB	10:1	-703.2	171.0
Al/SD255	1:1	-593.6	193.2
Al/SD255	10:1	-518.9	276.1
NAB/Type 316L SS	1:1	116	-1.705
NAB/Type 316L SS	10:1	134.7	-14.47
NAB/SD255	1:1	163.1	-64.29
NAB/SD255	10:1	185.3	-38.88

TABLE 2. GALVANIC CURRENT AND POTENTIAL MEASUREMENTS AT 24 °C

Galvanic Couple (Anode/Cathode)	Area Ratio	Couple Potential (mV)	Galvanic Current Density ($\mu\text{A}/\text{cm}^2$)
Al/Type 316L SS	1:1	-774.8	148.9
Al/Type 316L SS	10:1	-698.8	123.9
Al/Type 316L SS	1:10 ^(A)	-356.0	391.9
Al/NAB	1:1	-557.4	142.1
Al/NAB	10:1	-708.2	129.9
Al/NAB	1:10 ^(A)	-482.6	486.0
Al/SD255	1:1	-431.3	224.0
Al/SD255	10:1	-532.5	223.4
Al/SD255	1:10 ^(A)	-328.8	699.7
NAB/Type 316L SS	1:1	42.62	-1.189
NAB/Type 316L SS	10:1	-94.40	0.913
NAB/SD255	1:1	277.3	-89.50
NAB/SD255	10:1	31.90	-93.84
NAB/ D255	1:10	177.3	-36.81

^(A)1:10 ratio tests were performed only at 24 °C.

the galvanic corrosion of aluminum changed only very slightly with an increasing aluminum anode area. These results indicate that the galvanic corrosion of the

aluminum anode in this system is primarily cathodically controlled. Thus, larger sacrificial aluminum anodes are recommended in this scenario.

Galvanic currents in many situations are proportional to the surface area of the cathode. In this study, the galvanic corrosion of aluminum increased with a higher cathode (SD255).

Galvanic corrosion testing showed that there is no significant galvanic effect between SD255 and NAB. Similarly, no significant galvanic corrosion occurred between Type 316L SS and NAB. This outcome indicates that the galvanic effect does not influence the corrosion of NAB observed in seawater.

Conclusions

1. Relative CDs measured at an anode/cathode area ratio of 10:1 were not significantly higher than the currents measured at an anode/cathode area ratio of 1:1.
2. Aluminum anodes (1000 series) coupled with SD255, at 4 °C and 24 °C, and aluminum anodes coupled with NAB, at 4 °C, exhibited higher galvanic corrosion CDs compared to aluminum coupled with Type 316L SS.
3. No significant galvanic corrosion was observed between SD255 and NAB. Similarly, no significant galvanic corrosion occurred between Type 316L SS and NAB.
4. Test results indicate that the galvanic corrosion of the aluminum anode in this system is primarily cathodically controlled. Thus, larger sacrificial aluminum anodes are recommended in this scenario.

References

- 1 S. Divi, M. Gould, D. Efirid, "Galvanic Current Density Measurements of Anode for Subsea Vibration Data Logger (SVDL) System," CORROSION 2021, paper no. 16717 (Houston, TX: NACE International, 2021).
- 2 ASTM G71-81 (Reapproved 2019): "Standard Guide for Conducting and Evaluating Galvanic Corrosion Tests in Electrolytes" (West Conshohocken, PA: ASTM International, 2019).
- 3 <https://www.stress.com/capabilities/upstream/instrumentation-and-data/ss-data-logger>.
- 4 <https://www.hartenergy.com/exclusives/monitoring-riser-and-wellhead-fatigue-177133>.

- 5 S. McNeill, et al., "Drilling Riser Fatigue Monitored in Real Time Aboard Drillship," *World Oil*, March (2013): pp. 53-59.
- 6 F.E. Varela, Y. Kurata, N. Sanada, "The Influence of Temperature on the Galvanic Corrosion of a Cast Iron/Stainless Steel Couple (Prediction By Boundary Element Method)," *Corros. Sci.* 39, 4 (1997): pp. 775-788.
- 7 R. Francis, "Galvanic Corrosion of High Alloy Stainless Steels in Sea Water," *British Corrosion J.* 29,1 (1994): pp. 53-57.
- 8 R. Francis, *Galvanic Corrosion: A Practical Guide for Engineers*, 1st ed. (Houston, TX: NACE, 2001).

SURESH DIVI is a senior associate at Stress Engineering Services, Inc. Corrosion Technology Center (CTC), Houston, Texas, USA. He primarily provides corrosion engineering support for oil and gas (upstream, mid-stream, and downstream) and chemical process industry sectors. His major work at CTC involves designing and supervising in-house corrosion testing projects, standards (NACE/ASTM), and customized testing according to the clients' requirements. His areas of testing include standard immersion, flow effects on corrosion (jet impingement testing), packer fluid corrosion, drilling fluid corrosion, acidizing corrosion control, HPHT production corrosion, corrosion inhibitors, electrochemical (alternating current and direct current) corrosion, OLI, NORSOK corrosion modeling, and development of non-standard corrosion test techniques. Divi has earned a Ph.D. and Texas PE. He has been a member of NACE International (now AMPP) for 18 years.

MELISSA GOULD is a principal at Stress Engineering Services, Inc., Houston, Texas, USA, email: melissa.gould@stress.com. She has spent over 30 years performing detailed engineering of subsea pipeline and equipment, including cathodic protection designs and assessments, and has overseen component fabrications and installations.

DAN EFIRD is a subject matter expert at Stress Engineering Services, Inc. **MP**

TABLE 3. GALVANIC CORROSION RATE AT 4 °C AND 24 °C

Galvanic Couple (Anode/Cathode)	Area Ratio	Galvanic Corrosion Rate (mm/year)	
		at 4 °C	at 24 °C
Al/Type 316L SS	1:1	1.9	2.7
Al/Type 316L SS	10:1	2.3	3.0
Al/NAB	1:1	2.6	2.8
Al NAB	10:1	2.1	3.1
Al/SD255	1:1	3.5	4.1
Al/SD255	10:1	3.6	4.1
NAB/Type 316L SS	1:1	0.00	0.01
NAB/Type 316L SS	10:1	0.20	0.00
NAB/SD255	1:1	0.00	0.00
NAB/SD255	10:1	0.00	0.00

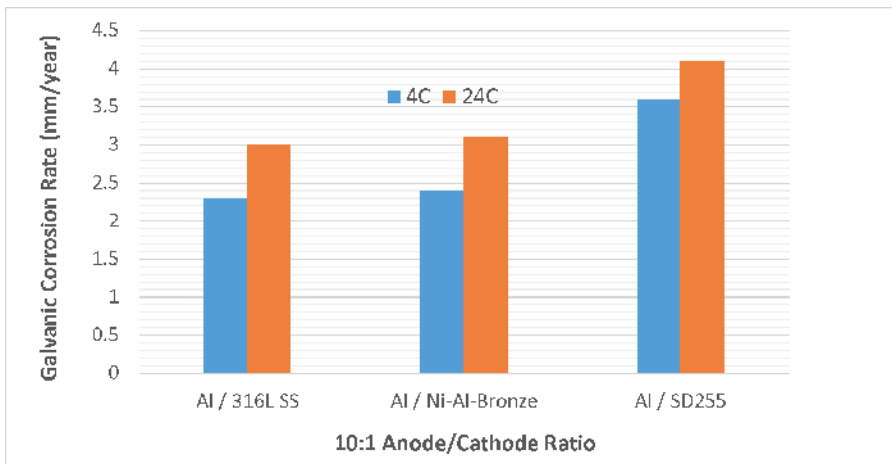


FIGURE 4 Galvanic corrosion rates with anode/cathode ratio of 10:1.

DID YOU KNOW....

The New AMPP YouTube channel brings you the latest news and information about corrosion, coatings, asset protection, AMPP education, certification, conferences, events and much more!

youtube.com/c/AMPPorg

